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Osmosis-induced swelling of Eurobitum bituminized radioactive waste in constant total stress conditions

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ABSTRACT

In geological disposal conditions, contact of Eurobitum bituminized radioactive waste, which contains high amounts of the hygroscopic and highly soluble NaNO₃, with groundwater will result in water uptake and swelling of the waste, and in subsequent leaching of the embedded NaNO₃ and radionuclides. The swelling of and the NaNO₃ leaching from non-radioactive Eurobitum samples, comprised between two stainless steel filters and in contact with 0.1 M KOH, was studied in restricted (semi-confined) swelling conditions, *i.e.* under a constant total stress, or counterpressure, of 2.2, 3.3, or 4.4 MPa (*i.e.* oedometer conditions). Four tests were stopped after hydration times between 800 and 1500 days, and the samples were analyzed by micro-focus X-ray Computer Tomography (µCT) and by Environmental Scanning Electron Microscopy (ESEM). The complete set of data enabled a consistent interpretation of the observations and lead to an improved understanding of the phenomenology of the water uptake, swelling, and NaNO3 leaching in restricted swelling conditions. Under the studied conditions, the bituminous matrix surrounding the NaNO₃ crystals and pores with NaNO₃ solution behaved as a highly efficient semipermeable membrane, *i.e.* osmotic processes occurred. In the main part of the leached layers, a high average NaNO₃ concentration and related to this a high osmotic pressure prevailed, explaining why in the studied range the swelling was not measurably affected by the counterpressure. At the interface with the stainless steel filters, a low permeable re-compressed bitumen layer was formed, contributing to the slow release of NaNO3 compared to the water uptake rate. A fully coupled Chemo-Hydro-Mechanical (CHM) constitutive model has been developed that integrates the key processes involved and that reproduces satisfactorily the results; this is presented in another work. Combination of the experimental and the modelling study allow to conclude that under semi-confined conditions the swelling of the bituminized waste, and its evolution with time, is the result of several transient processes (salts dissolution, diffusion of salts and water, advection, creep, involving a low permeability material with evolving thickness and properties) that moreover are non-linear and strongly coupled.

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1. Introduction

Eurobitum intermediate level bituminized radioactive waste has been produced at the EUROCHEMIC/BELGOPROCESS reprocessing facility (Mol-Dessel, Belgium), to immobilise precipitation sludge and evaporator concentrates originating from the chemical reprocessing of spent nuclear fuel and cleaning of high level waste storage tanks. Eurobitum consists of ~60 weight% (wt%) of 'hard' (also called 'blown' or 'oxidized') bitumen (Mexphalt R85/40) and ~40 wt% of waste. NaNO₃ and CaSO₄ are the most abundant salts

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and make up respectively 20–30 wt% and 4–6 wt% of the bituminized waste (BW). The waste further contains CaF_2 , $Ca_3(PO_4)_2$, $Ni_2[(Fe, Mn)(CN)_6]$, and oxides and hydroxides of Fe, Zr, and Al (4–10 wt%). Radionuclides are estimated to be present but for some 0.2 wt% at most [1,2]. All these salts, precipitates, and (hydr)oxides are finely dispersed in a matrix of bitumen (Fig. 1).

The current reference solution pursued by the Belgian Agency for the Management of Radioactive Waste and Fissile Materials (ONDRAF/NIRAS) envisages the direct underground disposal of Eurobitum in a geologically stable clay formation [3]. The Boom Clay, which is a 30–35 million years old and ~100 m thick marine sediment, is presently being studied as a reference host formation because of its favourable properties to limit and delay the migration of the leached radionuclides over extended periods of time [4]. When not disturbed, the Boom Clay will thus delay and spread





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Fig. 1. SEM photograph of Eurobitum bituminized radioactive salts. Both smaller (\emptyset 2–3 µm) and larger (\emptyset 15–20 µm) NaNO₃ crystals, as well as other salts, precipitates, and (hydr)oxides, are homogeneously dispersed in a matrix of bitumen. Note that the bitumen matrix is almost 'saturated' with the waste substances. Energy-Dispersive X-ray (EDX) analyses show that even the places that apparently consist of 'pure' bitumen contain NaNO₃ and CaSO₄.

in time the migration of the radionuclides, allowing the majority to decay before reaching the aquifers. Several 220 l drums, filled with \sim 170 l of Eurobitum, would be grouped in thick-walled concrete 'secondary' containers, which in turn would be placed in concrete-lined disposal galleries that are excavated at mid-depth in the clay layer. The remaining voids between the containers would be backfilled with a cement-based material.

A good understanding of the long-term behavior of Eurobitum in underground disposal conditions is an absolute prerequisite in view of its safe geologic disposal. Amongst the processes of concern, the interaction of the bituminized waste with clay pore water is of particular importance [2,5]. NaNO₃ is a very hygroscopic and deliquescent salt: it will strongly absorb large amounts of water or water vapour from the environment it is exposed to, resulting in the formation of an aqueous solution (*i.e.* deliquescence) [6]. The bitumen that surrounds the salt crystals has a very low permeability to water, but its ability to restrict the movement of dissolved ions even more makes it behave as a highly efficient semi-permeable membrane [7,8]. As a result, contact of the bituminized waste with water will result in an osmosis-induced swelling of the waste [9–14]. If (further) swelling is hindered, the swelling Eurobitum will exert a high 'osmotic' (i.e. osmosis-induced) pressure on its surroundings [10,14-16] (see Appendix A). In addition to the dissolution of NaNO₃, anhydrous calcium sulfate ('natural anhydrite'; solubility ~0.015 mol/L (M); density ~2.96 g/ml) can recrystallise with 0.5 water molecules to 'Paris Plaster' (solubility ~0.21 M; density \sim 2.74 g/ml) or with two water molecules to gypsum (solubility \sim 0.014 M; density \sim 2.32 g/ml), also resulting in a volume and/or pressure increase. High swelling-induced deformation and stresses could thus lead to a mechanical disturbance and possibly damage of the surrounding host formation [17], of which the consequences in terms of barrier performance have to be assessed.

To better understand these processes, and to enable to predict the long-term behavior of Eurobitum in underground disposal conditions, ONDRAF/NIRAS launched a large research programme. At the Belgian Nuclear Research Centre SCK-CEN water uptake experiments in constant volume and constant total stress (or: constant counterpressure) conditions are performed, and the influence of several parameters (NaNO₃ content in the BW and in the leachant, and degree of ageing) is investigated. Simultaneously, the International Centre for Numerical Methods and Engineering (CIMNE, Polytechnical University of Cataluña, Barcelona, Spain) started developing a fully coupled chemo-hydro-mechanical constitutive model for Eurobitum that considers the coupled osmotic flow and ultrafiltration [18]. The first results of the experimental programme were reported in [14,16]. In this paper, we report new experimental results on swelling, NaNO₃ leaching, and characterisation of leached samples, for the constant total stress tests. Before proceeding, we briefly summarize the present insights in the phenomenology of the water uptake and swelling in free swelling conditions.

2. Phenomenology of the water uptake and swelling in free swelling conditions

The phenomenology of the water uptake, swelling, and salt leaching processes in free swelling conditions is now reasonably well understood [8,10–13]. For a BW like Eurobitum, with a waste loading of \sim 40 wt% and with a NaNO₃ content between 20 and 30 wt%, the processes occurring in unconfined conditions, *i.e.* where free swelling is possible, can be described in a simple way by considering a binary mixture of bitumen and NaNO₃ (Fig. 2). In contact with water, the NaNO₃ salt crystals at the surface (see also Fig. 1), which are not covered by a layer of bitumen, will dissolve rapidly in the contacting solution. Water will also diffuse slowly through the bitumen that surrounds the NaNO₃ crystals in the layer just underneath the outer bitumen layer - which (initially) acts as a highly efficient semi-permeable membrane¹ – and start to dissolve these NaNO₃ crystals. This results in the formation of pores filled with a mixture of undissolved NaNO₃ in contact with a saturated NaNO₃ solution (7.8457 mol/dm³ at 25 °C, [19]). The water activity² of this mixture, as well as the water activity of a saturated NaNO₃ solution, is 0.74. As the volume of the NaNO₃-H₂O mixture is larger than that of NaNO₃, this layer of the BW swells.

Because the diffusion of water through the bitumen in the BW is a slow process, most of the water that is taken up further by the BW stays in the 'first' layer of pores, to dissolve the remaining NaNO₃ crystals and, in a next step, to dilute the saturated NaNO₃ solution. As a result, big pores filled with gradually less concentrated NaNO₃ solution – and thus with gradually increasing water activities – appear in the outer BW layer [12]. A small part of the water that is taken up diffuses deeper into the BW, until it reaches the next NaNO₃ crystals to be dissolved and diluted, contributing in turn to the swelling. This fraction of water diffusing deeper into the BW increases as the water activity in the first layer becomes higher than 0.74, which is achieved when all NaNO₃ crystals are dissolved and the saturated NaNO₃ solution starts to dilute.

The swelling of the BW as a result of the water uptake modifies, by the high stretching of the bitumen, the membrane properties of the surrounding bitumen (rather: bituminous matrix, see below), making it gradually more permeable to the dissolved salts, *i.e.* the bitumen behaves increasingly less as a highly efficient semipermeable membrane. In addition, at high swelling degrees, the NaNO₃ solution filled pores may become interconnected. This way, a continuously growing permeable layer consisting of connected pores is created. As a result, NaNO₃ can leach from the BW. It is to be noted that it is likely that in BW the omnipresence of the waste compounds (soluble and sparingly soluble salts, (hy-dr)oxides, ...; Fig. 1) creates already from the start a low-porosity

¹ The efficiency of a material to behave as a semi-permeable membrane, *i.e.* the osmotic efficiency, is calculated as the ratio of the measured osmotic pressure and the theoretical osmotic pressure if the material were an ('100%') ideal semi-permeable membrane (*e.g.* S.J. Fritz, Ideality of clay membranes in osmotic processes: a review, Clays and Clay Minerals 34 (2) (1986) 214–223). Accordingly, a highly efficient semi-permeable material refers to a material with a high osmotic efficiency.

² The water activity is defined as the ratio of the water vapour pressure of a salt solution and the water vapour pressure of pure water. This value is temperature-dependent.



Fig. 2. Simplified schematic representation of the water uptake and swelling in a binary bitumen – NaNO₃ mixture in free swelling conditions. (a) Dry mixture of bitumen and NaNO₃ crystals. (b) Mixture in which in the first layers the NaNO₃ crystals are partially or completely dissolved (to an oversaturated, saturated, or undersaturated solution). (c) Mixture with layers of large pores with (more) diluted solution, and small pores with (more) concentrated ((over, under)saturated) NaNO₃ solution. \Box = dry NaNO₃ crystal, \bigcirc = pore with NaNO₃ solution. \downarrow refers to the direction of water taken up by the material, $\uparrow\uparrow$ refers to the direction of the swelling.

network for water [20], and possibly for dissolved salts, thus increasing the permeability and decreasing the efficiency of bitumen as a semi-permeable membrane.

Two important remarks apply to this description. Firstly, the waste loading is an important parameter governing the swelling and soluble salts leaching. For waste loadings of \sim 50 wt% and higher, an increasing part of the mineral particles in the waste is no longer fully covered by a layer of bitumen, and the leaching of soluble salts such as NaNO₃ increases drastically (this is the so-called percolation effect [21,22]). It is likely that in such case the osmosis-induced swelling of the waste will be small to unexisting. Secondly, ageing by radiooxidation processes results in the hardening and embrittlement of bitumen [23–25]. This is expected to decrease the efficiency of bitumen as a semi-permeable membrane, and hence to result in a lower swelling degree and a higher NaNO₃ leaching. It can be noted here that the increase in the asphaltene fraction of the aged bitumen could have a positive effect on the radionuclide containment properties of the bitumen matrix [25].

The description of the water uptake, swelling, and NaNO₃ leaching processes as described above is valid for free swelling conditions. In geological disposal conditions free swelling will only be possible during a first phase, until the free volume in a 2201 drum is filled with swollen Eurobitum (assuming that this free volume will remain available during the whole free swelling phase). According to our calculations on the basis of results reported in [9,10], this could already be the case a few 100 years after contact with water. Once there is no more space for further swelling, the swelling Eurobitum will exercise an osmosis-induced pressure (see Appendix A), in first instance on the concrete secondary container, but finally on the surrounding clay formation. As a result, the surrounding clay will be slowly deformed, giving additional space for Eurobitum to swell. Due to its deformation, the counterpressure exerted by the clay will increase with the further swelling of the Eurobitum, *i.e.* a stress redistribution in the clay will occur. As long as the osmosis-induced pressure of the swelling Eurobitum can exceed the counterpressure exerted by the Boom Clay, swelling will go on. For characterisation and constitutive model development purposes, the tests that are reported in this paper are performed under different constant stress (oedometric) conditions, aiming at simulating various stages of the system evolution.

3. Experimental aspects

3.1. Non-radioactive reference Eurobitum and gamma irradiation

Non-radioactive reference Eurobitum was sampled from drum '0-2 CR15/16' that was produced during the 'cold runs (CR)' of EUROCHEMIC's bituminization installation in the 1970s (Table 1). The production method and composition of this non-radioactive reference Eurobitum are entirely similar to that of the radioactive Eurobitum, except for the presence of the radionuclides (less than 0.2 wt% in the real waste [1,2]).

Ring-shaped samples (inner diameter and height = 200 mm and 9-10 mm, respectively; outer diameter and height = 300 mm and 10-12 mm, respectively) of the non-radioactive reference Eurobitum were first gamma-irradiated in the absence of oxygen, to simulate the internal alpha-beta-gamma irradiation that a subsurface layer of the Eurobitum (i.e. a layer that is not contacted by water in the free swelling phase) experiences during interim storage and underground disposal until it comes in contact with water. Dose rates were higher than in the industrially produced radioactive Eurobitum, and varied between 150 Gy/h and 130 Gy/ h, to deliver a total absorbed dose of ~750 kGy. Experimental details and results and discussion are given in [23,24]. Considering that for the hard (blown, oxidized) Mexpalt R85/40 the vield of radiolytically produced H_2 is about three times higher under alpha irradiation than under beta/gamma irradiation [2], we assume that the ageing effect of a dose of \sim 750 kGy corresponds to that of an alpha (\sim 200 kGy) and beta–gamma (\sim 100 kGy) dose absorbed after about 200 years. Scoping calculations indicated that for a disposal gallery in Boom Clay Eurobitum will come in contact with pore water within 100 years after closure of the disposal gallery [26].

3.2. Filling of the water uptake cell with gamma-irradiated Eurobitum

The laboratory tests to study the processes related to the water uptake by Eurobitum make use of water uptake cells that are placed in oedometers (Fig. 3).

The water uptake cells consist of three parts:

Table 1

Characteristics of the non-radioactive reference Eurobitum used in this study (data obtained from EUROCHEMIC/BELGOPROCESS).

Identification code	Wt% salts	Wt% NaNO3 ^a	Wt% H ₂ O	Density (g/ml)
0-2 CR15/16	38.9	28.5	0.39	1.31
Production date	Vol% salts	Vol% NaNO ₃	Vol% other in	norganic material
11/01/1977	23	17	6	

^a Destructive chemical and non-destructive Neutron Activation Analysis of subsamples from the drum, taken from the zone where the samples for the water uptake tests where sampled, indicate that the NaNO₃ content in this drum is rather ~31 wt%. On the basis of linear extrapolation, the density of the material would be rather 1.33 g/ml.



Fig. 3. Schematic visualization of the experimental set-up for water uptake tests with Eurobitum samples (diameter 38 mm, height 10 mm), contacted at both sides with 0.1 M KOH (SA/V = 0.32 or 0.45 mm⁻¹; see text) that is regularly sampled and renewed to maintain the water activity above 0.98. Note that the two solution compartments (for the two filters) are connected, assuring nearly the same water activity in both filters.

- (i) a bottom plate with sintered stainless steel filter that supports the Eurobitum sample,
- (ii) a movable piston with sintered stainless steel filter that contacts the upper surface of the Eurobitum sample, and
- (iii) a 'holder' that is fixed with eight screws on the bottom plate, and that contains the filters, the Eurobitum sample, and the piston, so as to force the swelling of the Eurobitum sample in one (upwards) direction.

The average pore diameter of the sintered stainless filter is $3.2 \,\mu$ m, with a pore distribution range between 1.5 and 5 μ m. Behind the filters, a 2 mm wide coiled channel that is connected with the small diameter ingoing and outgoing stainless steel tubes maximises the equilibration between the leached salts in the filter and the leachant. The holder is conceived in such a way that it also allows the cutting of the Eurobitum sample out of a larger sample without having to heat the sample. This avoids that the internal structure of the gamma-irradiated sample, which might influence the kinetics of the studied processes, is destroyed (*e.g.* the porosity caused by the radiolytic H₂ generation during the irradiation).

3.3. Loading-unloading test with the dry Eurobitum

After cutting the Eurobitum sample (38 mm diameter, variable height) out of a 50 mm diameter and 9–12 mm thick gammairradiated sample (Section 3.1), the piston with filter was introduced and the cell was placed in a front loader oedometer and submitted to two loading/unloading cycles. These loading/unloading steps allowed (i) to press the samples to a constant thickness of ~10 mm and to get a good contact between the sample on the one hand and the wall of the holder and the two filters on the other hand (first loading/unloading step), and (ii) to characterise the mechanical behavior of the bitumen samples (second loading/ unloading step). The displacement of the piston was followed with a dilatometer (see below). For each loading step, an instantaneous volumetric deformation was followed by creep (*i.e.* a slow delayed deformation) [27,28]. For high stress levels (≥ 2.2 MPa) volumetric creep deformations disappeared because the pore volume became negligible, and the material showed only a volumetric elastic response. However, under a high pressure, part of the bitumen or BW flowed into the pores of the sintered stainless steel filters and into the tiny void between piston and holder. This may have contributed to the observed creep.

The maximum stresses that were applied were 2.2, 3.3, or 4.4 MPa. These are the stresses that were to be applied during the subsequent water uptake tests. Values of 2.2 and 4.4 MPa are representative for respectively the hydrostatic pressure and the total pressure in the undisturbed Boom Clay at a depth of -220 m. Also during the second loading/unloading test, a continuous but slow negative displacement of the piston was observed, pointing to the flowing of bitumen in the filter pores and in the void between piston and holder. In total, eight stainless steel water uptake cells were prepared this way, labelled S0, S1, ..., and S7.

3.4. Follow-up of swelling and NaNO₃ leaching

When the target stress of 2.2, 3.3, or 4.4 MPa on the BW samples was attained, 0.1 M KOH was introduced in the water circuit of the water uptake cell. A 0.1 M KOH solution was chosen to simulate to some extent so-called 'young cement water' – which is the first percolation water of concrete [29] – as in repository conditions the bituminous waste will be surrounded by cementitious materials. Young cement water contains a low Ca(OH)₂ concentration and high concentrations of NaOH and KOH, which are present as impurities in cement. To allow to monitor the leaching of Na⁺, only KOH was used.

To assure that all air bubbles were removed, especially those in the edges and adsorbed on the filter material, the solution supply circuit was extensively and repeatedly rinsed with the 0.1 M KOH solution. Under normal operation conditions (*i.e.* no replacement of the leachant), the pressure on the 0.1 M KOH solution was maintained between 0.2 and 0.15 MPa (2 and 1.5 bar) absolute. It has to be noted that this liquid pressure is considerably lower than the hydrostatic pressure of 2.2 MPa prevailing in the Boom Clay at a depth of -220 m. As a result, the total effective stress on the sample, which is the difference between the total (vertical) stress and the liquid pressure, was close to the total stress. The SA/V ratio, this is the ratio of the geometrical external surface area of the Eurobitum sample that is in contact with the leachant and the leachant volume, was for five tests 0.45 mm^{-1} (surface: 22.7 cm²; leachant volume: 5 cm³). For three tests a pipette was included in the water supply circuit (not shown in Fig. 3), aimed at monitoring the uptake of solution by the sample. For these tests, the SA/V ratio was 0.32 mm⁻¹ (\sim 7 cm³ of leachant).

The swelling of the samples in these constant stress tests was followed by measuring the displacement of the piston with a digital dilatometer that was connected to a data acquisition system that continuously measured the position of the piston. In general every 4–6 h, a measurement value was saved. Before the start of the experiments, each of the eight measurement chains was calibrated according to the ISO/IEC 17025 guidelines. The resolution of the dilatometers is 0.01 mm, the combined uncertainty on the displacement measurements is ~0.015 mm (95% confidence). Almost immediately after the injection of 0.1 M KOH, a clear positive displacement due to the flowing of the BW in the filter pores and void between piston and holder is thus completely obscured by the swelling of the BW. The leaching of NaNO₃ was followed by replac-

ing the leachant with 10 cm³ of fresh 0.1 M KOH solution at times $t = (2 \cdot x)^2$, with $x = 1, 2, 3, \dots$, with t in days (*i.e.* sampling occurred 4, 16, 36, ... days after the start of the hydration). This sampling sequence was chosen because it is well-known that the uptake of water and the leaching of NaNO₃ from bituminized waste in free swelling conditions is reported to be a diffusion-controlled process [8-16]. The regular renewal of the leachant according to this sampling sequence was expected to enable to limit NaNO₃ concentration differences in the leachant. Measured NaNO₃ concentrations proved to vary between 0.05 and 0.3 M, thus maintaining the water activity of the leachant (0.1 M KOH + 0.05–0.3 M NaNO₃) above 0.98. At these high water activities, the water uptake rate is close to its maximal value [8,12], whilst meanwhile the tests are performed for a realistic, although somewhat low NaNO₃ concentration [26]. The sampling and renewal of the leachant had no measurable effect on the position of the piston. The sampled solutions were first weighed and recalculated to volume using a density of 1 g/ml, and then analyzed by Inductively Coupled Plasma Atomic Emission Spectroscopy (ICP-AES) and Ion Chromatography (IC), to measure the concentrations of Na⁺ and Ca²⁺, and nitrate and sulfate, respectively. Combination of the sampled volumes of leachant and the ion concentrations in the leachant allows to calculate the amount of NaNO₃ leached from the Eurobitum.

To demonstrate that osmosis is the key process governing the water uptake and swelling of Eurobitum BW, the 0.1 M KOH solution in one water uptake cell (cell S1) was replaced by a nearly saturated NaNO₃ solution (a saturated NaNO₃ solution was prepared at 15 °C, and then used at ~23 °C), ~1000 days after the start of the water uptake experiment. After ~1200 days, this nearly saturated NaNO₃ solution. During the contact with this solution, the leachant was not sampled. After ~1360 days, the nearly saturated solution was replaced by a fresh 0.1 M KOH solution. From that time onwards, the leachant was sampled monthly to quickly reach low NaNO₃ concentrations in the leachant.

3.5. End of the test – dismantling of the water uptake cells – analyses

Between \sim 800 and \sim 900 days after the start of the water uptake tests, three tests were stopped and dismantled. A fourth test was stopped after \sim 1500 days. To minimise the disturbance of the partially leached Eurobitum samples when retrieving the water uptake cells from the oedometers (removal of stress) and when pushing the samples out of the water uptake cell (high stress by means of a small press), the water uptake cells were first gently sprayed with liquid nitrogen until the Eurobitum samples were frozen. This procedure was first successfully tested on a water uptake cell containing a sample composed of an 8 mm thick partially leached sample that was sandwiched between two fully leached samples of 1 mm thickness. After retrieval, the frozen samples were first analyzed by micro-focus X-ray Computer Tomography (µCT). This analysis technique detects differences in attenuation of X-rays in the material, which are related to different densities, and hence allows to distinguish the leached and unleached zone. The resolution of this technique depends on the characteristics of the apparatus and on the distance between the sample and the detector (and thus on the size of the sample). The obtained µCT images have a voxel (volume element) size of about 94 µm, hence the resolution is 188 µm. Further details of the procedure and the interpretation of the results are given in [30].

Next, the samples were slowly heated to ambient temperature, and a razor blade was used to carefully separate the two filters from the sample. The sample itself was stored again at -20 °C immediately after removal of the filter. Probably because bitumen had flown into the filter pores, small and sometimes irregular parts of the outermost leached layers remained stuck on the filters and

were thus withdrawn from the samples. The leached BW that remained stuck on the filters was carefully removed. Next, the filters were placed in a beaker with carbon tetrachloride (CCl₄) to dissolve the bitumen that during the test had penetrated in the filter pores. This washing procedure was repeated until all bitumen was leached from the filter. After evaporation of the CCl₄, the remaining bituminous phase was weighed to finally calculate the volume of bitumen that filled the pores of the filters.

Finally, the samples were frozen again before they were broken in two half-cylindrical parts by means of hammer and chisel. The central part of the fractured surface of one half-cylindrical part was then analyzed from top to bottom (*i.e.* from the utmost leached part at the upper filter to the utmost leached part at the lower filter) by Environmental Scanning Electron Microscopy (ESEM), to study the depth of water penetration and dissolution and leaching of NaNO₃. The resolution of this technique for our conditions was ~2 μ m.

4. Results and discussion

4.1. Swelling of the BW samples

Fig. 4 shows the evolution of the displacement of the piston, *i.e.* the swelling, for the gamma-irradiated Eurobitum samples, under constant total stresses of 2.2, 3.3, or 4.4 MPa, when they are hydrated with 0.1 M KOH (and, for cell S1, with a nearly saturated NaNO₃ solution in the period 1019–1354 days and in a second period starting at 1670 days) under a solution pressure between 2 and 1.5 bar absolute, as a function of time. The swelling degree (expressed in percent) is calculated from these results as

$$\frac{(h-h_0) \times \pi \times r^2}{h_0 \times \pi \times r^2} \times 100 = \frac{(h-h_0)}{h_0} \times 100$$
(1)

with h and h_0 the height of the swollen and the dry sample, respectively, and r the radius of the sample.

Several observations can be made. Firstly, it is seen that after more than 4 years of contact with 0.1 M KOH, all (remaining) samples continued to swell, with nearly no tendency to level off. For a water pressure of the leachant between 1.5 and 2 bar absolute, five of the eight samples swell(ed) at a rate of ~250 μ m/year (~2.5 vol%/year, for both sides of the sample in contact with solution), independently of the applied stress. It should be stressed that



Fig. 4. Evolution of the (uni-axial) swelling of gamma-irradiated EUROBITUM samples at both sides in contact with 0.1 M KOH, which is regularly renewed to maintain the water activity above 0.98. The samples are allowed to swell against a constant stress of 2.2, 3.3, or 4.4 MPa (see Fig. 3). The uncertainty on the swelling measurements is 0.015 mm (95% confidence). From top to bottom: Cell S2 (2.2 MPa, +pipette (P)), S5 (4.4 MPa, +P), S7 (3.3 MPa, +P), S3 (4.4 MPa, -P), S0 (2.2 MPa, -P; note that the curve for this cell (stopped after 886 days) is mostly hidden behind the curve for S3); S6 (3.3 MPa, -P), S1 (2.2 MPa, -P), and S4 (4.4 MPa, -P; note that the curve for S1). These eight tests were not started at the same day.

Table 2
Summary of data on swelling of the BW samples in constant stress conditions.

Identification code	Duration (days)	Initial sample thickness (mm) ^a	Measured piston displacement (mm)	Equivalent height due to BW in filters (mm)	Corrected piston displacement (mm)	Volume increase (ml) ^b	Volume increase (%)
S0 (2.2 MPa, -P)	887	9.33	0.63	0.10	0.73	0.71-0.83	6.7-7.8
S4 (4.4 MPa, -P)	872	9.42	0.52	0.11	0.63	0.59-0.71	5.5-6.7
S5 (4.4 MPa, +P)	1472	9.33	1.40	0.09	1.49	1.59-1.69	15-16
S7 (3.3 MPa, +P)	805	9.83	0.78	0.15	0.93	0.89-1.05	8.0-9.5

^a Based on µCT measurement, and including the contribution of BW in the filter.

^b Calculated with respect to the measured and corrected piston displacement, respectively.

the measured swelling degrees are systematically smaller than the 'real' swelling degrees, due to the penetration of some BW into the filter pores. For the tests that were stopped after \sim 800–1472 days, the amount of bitumen or BW that thus did not contribute to the displacement of the piston – as determined by washing with CCl₄ - corresponded with a 'missed' piston displacement of \sim 0.09 to \sim 0.12 mm. In other words, if BW did not flow into the filter pores, the real swelling after this time would have been by up to 20% higher than the measured values. The total volume increases are summarized in Table 2. As it is not known when the BW was pressed into the filter pores (during the compressibility test, during the water uptake test, or both), the total volume increases were calculated on the basis of the piston displacement, either measured as such or corrected for the contribution of the BW in the filter pores. The values range from 0.6 to 1.7 ml (initial sample volume \sim 10.6 ml), or \sim 5 to \sim 16 vol%. These values are higher than the maximum volume increase due to the recrystallization of anhydrous calcium sulfate ('natural anhydrite'; density ~2.96 g/ml) to gypsum (density ~ 2.32 g/ml), which is only ~ 0.15 ml for a 10 mm thick sample. This is a clear indication that the swelling of bituminized salts is not only due to salts recrystallization, and that osmosis, involving the dissolution of dry NaNO₃ and the further dilution of the NaNO₃ solution, as well as the presence of a highly efficient semi-permeable membrane, strongly contributes to the swelling.

For three samples, S2 (2.2 MPa, +pipette (P)), S5 (4.4 MPa, +P), and S7 (3.3 MPa, +P), swelling rates of 350-550 µm/year (3.5-5.5 vol%/year) were measured. These higher swelling rates were observed for those systems for which the SA/V ratio is 0.32 mm^{-1} , that is, for which the water supply circuit includes also a pipette to follow the volume of water taken up by the Eurobitum. However, the slight difference in NaNO3 concentration in the leachant due to the higher leachant volume and due to the slightly differing sampling procedure is too small to cause an effect on the swelling rate. This was among others confirmed by a test in nearly constant volume conditions where the leachant solution was not replaced during about 3 years (resulting in a NaNO₃ concentration of \sim 1 M instead of 0.05–0.3 M in the case of regular sampling), and where the regular renewal afterwards did not change the pressure increase rate [14]. In another constant pressure test, the pipette was closed from the system during several months during which no different swelling rates were observed. Therefore, it is more likely that the different swelling behavior is related to locally higher NaNO₃ contents in these samples, and/or to layers with a relatively higher content of smaller grains of NaNO₃.³ This was evidenced by the results on NaNO₃ leaching, which are discussed in Section 4.2. A variation of the salt content and/or the grain size in the BW is quite normal, since the industrial bituminization process does not allow to produce perfectly homogeneous waste products. For this reason, all samples destined for water uptake tests are now systematically scanned by μ CT, to check the homogeneity of the salts distribution.

A second important observation is that over the studied time period the swelling was not influenced by the counterpressure. This is clearly shown if the swelling degrees are plotted as a function of the counterpressure (Fig. 5; the three samples with a higher swelling degree, due to a higher NaNO₃ content (see Section 4.2), are not included in this figure). We believe that this is due to experimental counterpressures that are much smaller than the potential osmotic pressures in this system (see Appendix A). This is further discussed in Section 5.2.

Thirdly, it is seen that after a relatively short initial 'transition' stage, the swelling increased almost linearly with time, and not with the square root of time. At first sight, this is a somewhat surprising observation. On the basis of experimental results and mathematical approaches published in literature [8-12,15], we could expect the swelling to increase linearly with the square root of time, which is the normal behavior for a diffusion-controlled process such as the uptake of water by the BW. The results reported here, in combination with the insights obtained from the development of a constitutive law [27,28], suggest that in the constant stress conditions of our tests the ingress of water was not the (only) rate-limiting process, and that the swelling in these conditions is the overall result of several transient processes (diffusion, advection, dissolution, creep, involving a low permeability material with evolving thickness and properties) that moreover are nonlinear and strongly coupled.



Fig. 5. Relation between swelling and counterpressure for the water uptake cells without pipette, with presumably the same $NaNO_3$ content in the samples (S0 (2.2 MPa or 22 bar), S1 (2.2 MPa), S3 (4.4 MPa or 44 bar), S4 (4.4 MPa), and S6 (3.3 MPa or 33 bar)). Beyond 784 days, two of the five tests were stopped, making it impossible to follow the evolution of the relationship for longer contact times.

³ For an Eurobitum layer of 1 mm thick and 38 mm diameter, the NaNO₃ content is ~0.42 g (=28.5 wt%). If all of this NaNO₃ would be present as 1 µm diameter grains, such layer would contain 3.6×10^{11} grains of NaNO₃, and the thickness of the 'bituminous material' surrounding the NaNO₃ crystals (this is: the pure bitumen + sparingly soluble salts + (hydr)oxides of Fe, Zr, and Al; see Section 1) would be ~0.4 µm. If all of this NaNO₃ would be present as 10 µm diameter grains, the Eurobitum layer would contain 3.6×10^8 grains, and the thickness of the bituminous material around these grains would be ~4 µm.

For cell S1, it is seen in Fig. 4 that as a result of the replacement, after \sim 1000 days, of the 0.1 M KOH leachant by a nearly saturated NaNO₃ solution, the swelling rate fell down to almost zero. This is a clear demonstration that the water uptake and swelling of BW is to a large extent controlled by osmosis: since the water activity of the nearly saturated NaNO₃ solution was very close to the value of 0.74 for a saturated NaNO₃ solution or for dry NaNO₃, the difference of the water activity between the leachant and the saturated solution and dry NaNO₃ deeper in the BW sample became very small, and the water uptake process stopped. This also shows that the bitumen or bituminous material (as explained above) in these high counterpressure conditions continued to behave as a highly efficient semi-permeable membrane, even if it contained high amounts of non-bituminous material (~40 wt% or ~23 vol% of waste; see also Fig. 1 and Table 1). When examining the results in Fig. 4 in detail, it is seen that during the first \sim 50 days after the switch of the contact solution, a negative swelling, *i.e.* a contraction, occurred. This is due to the fact that immediately after the injection of the nearly saturated NaNO₃ solution the water activity gradient between filter and outer leached layer was switched from 'positive' (water flowing from the filter to the leached layer) to 'negative'. Because of this gradient switch, water moved from the low NaNO₃ concentration solution in the outermost layers of the leached BW (water activity \sim 0.98 or higher) to the high NaNO₃ concentration in the filter and tubings (water activity close to 0.74), whilst NaNO₃ diffused from the nearly saturated solution in the filter into the outermost BW layers, resulting in a negative swelling. With time, the NaNO₃ concentration in the filter and tubings increased again due to leaching from the sample, resulting in a zero water activity gradient, i.e. no more swelling or contraction. Replacement, after 1202 days, of the contacting solution with fresh nearly saturated NaNO₃ solution confirmed these findings: after a very short equilibration period due to the small but existing difference in water activity between the saturated NaNO3 solution in the whole leached layer and the nearly saturated NaNO₃ solution in the filter and tubings, the water uptake process stopped again. When after \sim 1360 days the saturated NaNO₃ solution was replaced by 0.1 M KOH, the swelling rate increased, as expected for an osmosis-driven process. In a first phase the swelling rate increased faster than at the start of the water uptake test. This is attributed to the (relatively) higher permeability of the swollen and partially leached layer of the BW sample compared to the low permeability of dry BW, which, despite the presence of a re-compressed low permeability layer at the contact with the filters (see Sections 4.4 and 5), facilitates the ingress of water into the partially leached layer of the BW. When due to the ingress of water the NaNO₃ concentration profile in the leached layer was again similar to the one before the switch to a nearly saturated NaNO₃ concentration, the water uptake rate decreased to its value before the switch. Due to a short but significant temperature variation ($\sim 4 \circ C$) and concomitant change of the swelling at \sim 1450 days – which is also visible for other the samples; note that the tests were not all started at the same day – the transition from a higher to a lower water uptake rate seems to be somewhat abrupt.

4.2. Leaching of NaNO₃

The bitumen (or the mixture of bitumen and sparingly soluble salts, (hydr)oxides, ...) surrounding the soluble salt crystals and the pores with salt solution is not a perfect semi-permeable membrane, and hence NaNO₃ (and other salts) can leach from the swelling BW. Fig. 6 shows the evolution of the cumulative amount of NaNO₃ that has leached out of the Eurobitum samples since the beginning of the experiments.

It is seen that just like the swelling the cumulative amount of leached NaNO₃ increased nearly linearly with time, in some cases



Fig. 6. Cumulative amount of NaNO₃ leached from the BW samples. The uncertainty on the cumulative leached amount of NaNO₃ is 10% (95% confidence).

after a short transition phase. As already discussed, this linear behavior is probably the combined result of different transient processes (diffusion, advection, dissolution, involving a low permeability material with evolving thickness and properties) that moreover are non-linear and strongly coupled. Since the sampling frequency was based on an expected diffusive behavior (see Section 3.4), the NaNO₃ concentration in the system between the different samplings (for which the duration between two consecutive sampling dates increased in the course of the experiment) was not constant but increased with the experiment running. Yet, in all cases the measured NaNO₃ concentrations varied between ~0.05 and ~0.3 M, corresponding with water activities of the leachate above 0.98, *i.e.* for which the effect on the water uptake and swelling rate is small [8,12].

The order of the curves for the cumulative amounts of leached NaNO₃ (Fig. 6) agrees well with that of the swelling, *i.e.* the higher the swelling, the higher the cumulative amount of leached NaNO₃ (Fig. 4). This agreement is shown graphically in Fig. 7. It is seen that the cumulative amount of leached NaNO₃ is linearly related to the swelling. This linear relationship is not unexpected. Whilst more water is taken up by the BW – either because the contact time with water increases (evolution with time) or because the BW contains layers with a locally higher NaNO₃ content and/or a different crystal grain size distribution, as for samples S2, S5, and S7 (see Footnote 3) – the BW continues to swell, and more NaNO₃ dissolves and leaches from the sample. The results for the three samples



Fig. 7. Relation between the piston displacement (~swelling) and the cumulative amount of NaNO₃ leached out of the studied Eurobitum samples, for the water uptake tests without pipette shown in Figs. 4 and 6.

S2, S5, and S7 that show a higher swelling (Fig. 4) and a higher cumulative amount of leached NaNO₃ (Fig. 6) fit well with the results for the five samples that show a more 'similar' behavior. This corroborates our interpretation that the higher swelling observed for these samples is due to the higher NaNO₃ content and/or to the relatively higher amount of small size grains in these samples, or at least in the leached layers of these samples. It has to be noted that this linear relationship is only valid for samples with a waste loading of \sim 40 wt% and a NaNO₃ content of, say, \sim 25 to \sim 35 wt%. Especially at waste loadings $\gtrsim 50$ wt% (*i.e.* the so-called percolation threshold [21,22]) the single mineral particles in the waste are no longer fully surrounded by a bitumen film. In such highly loaded BW, mineral clusters are present, which by the formation of interconnected pores severely increase the release rate of NaNO₃ and radionuclides, i.e. percolation effects. For such bituminized wastes, it is likely that the swelling - if any - and cumulative amount of leached NaNO₃ do not follow the linear relationship shown in Fig. 7.

In Fig. 7, for the five samples with similar swelling and NaNO₃ leaching behavior (S0, S1, S3, S4, S6; see Figs. 4 and 6), the upper points in the plot are related to the higher counterpressures (3.3 and 4.4 MPa), whereas the lower points in the graph are related to the lower counterpressures (2.2 and 3.3 MPa) (this is not shown in detail). Thus, in contrast to the (apparent) independence of the swelling on the counterpressure (Fig. 5), there seems to be for these five 'similar' samples a clear, yet small effect of the counterpressure on the cumulative leached amount of NaNO₃ This effect is visualized in Fig. 8. It is seen that a higher counterpressure resulted in a slightly higher cumulative leached amount of NaNO₃. A closer look at this figure indicates that this small difference was mainly created during the first ~250 days of the test, i.e. during the 'transition' period preceding the phase of (nearly) linear increase of the swelling (Fig. 4). The difference is possibly due to a larger NaNO₃ diffusion due to a slightly higher NaNO₃ concentration gradient



Fig. 8. Relation between the cumulative leached amount of NaNO₃ and the counterpressure for the water uptake cells without pipette, and with presumably the same NaNO₃ content (S0 (2.2 MPa or 22 bar), S1 (2.2 MPa), S3 (4.4 MPa or 44 bar), S4 (4.4 MPa), and S6 (3.3 MPa or 33 bar)).

Table 3

Summary of data on NaNO₃ leaching from the BW samples in constant stress conditions.

for the systems at 4.4 MPa (see Section 5.2) and/or a higher amount of BW flown into the filter with subsequently a higher amount of easily leached NaNO₃.

Since the initial NaNO₃ content in the samples is \sim 4.2 g (28.5 wt%, Table 1), Fig. 6 shows that after 1500 days, for all samples but one \sim 15 to \sim 25 wt% of the initial NaNO₃ content had leached (Table 3; these percentages can be 10-15% lower for a 10–15% higher initial NaNO₃ content, see footnote in Table 1). For the sample S2 even \sim 35 wt% of the NaNO₃ content had leached in this period, but as already mentioned, the NaNO₃ content in this sample, or in the leached layer of this sample, was probably higher than \sim 4.2 g (28.5 wt%). Since NaNO₃ is a very soluble salt, these are rather low values. This confirms again that in restricted swelling conditions (i.e. counterpressure on the swelling material), bitumen behaves as a highly efficient semi-permeable membrane, even when containing a high amount of inorganic compounds. The amounts of leached NaNO₃ correspond with a (hypothetical) fully leached BW layer with a thickness of \sim 0.9 to \sim 2.4 mm for both sides, or \sim 0.45 to \sim 1.2 mm for one side (Table 3). We define the thickness of this fully leached layer as the equivalent leached thickness. According to this definition, the BW adjacent to this fully leached layer is completely dry and unleached, *i.e.* the NaNO₃ content equals the initial NaNO₃ content. It is obvious that in reality the salt content in the leached layers is higher than zero, and that hence the thickness of the 'leached layer' (or: the layer of BW that is affected by the ingress of water, *i.e.* from dry NaNO₃ with no molecules of water to a saturated or undersaturated NaNO₃ solution) is larger than this equivalent leached thickness. As will be shown further below, µCT and ESEM are very interesting tools to estimate the thickness of the leached layer.

4.3. μ CT analysis of leached BW

The µCT images in Fig. 9 show the X-ray attenuation values in a slice perpendicular to the leachant surface of the Eurobitum BW samples of cell S0 (2.2 MPa, without pipette, 887 days) and S5 (4.4 MPa, with pipette, 1472 days). More µCT images can be found in [30]. The attenuation values are expressed as 16-bit integers (values between 0 and 2^{16} , *i.e.* values between 0 and 65,536). The full range of the colormap is used to visualize the attenuation values between 20,000 and 35,000 to improve the contrast in the µCT images and to better visualize the hydrated layers, as explained hereafter. The colour difference between both µCT images is due to the different tuning of the µCT apparatus for the two measurements. The apparent lower density in the centre of the sample in Fig. 9a is due to beam hardening, which is an artefact caused by the fact that the X-ray source of the µCT scanner emits polychromatic X-rays. The low energy X-rays of this spectrum are preferentially absorbed by the material, by which the effective energy of the beam increases as the beam penetrates deeper through the material. As a consequence, the outer part of an object seems to be denser than the inner part. Application of a hardware filter allows to decrease this effect, as seen in the right μ CT image [30]. For clarity, the discussion below mostly relates to Fig. 9b, but the same comments - taking into account the remarks above -apply also to Fig. 9a.

Code	Duration (days)	Cumulative amount of leached NaNO ₃ (g)	% leached (for 28.5 wt% of NaNO ₃ = 4.2 g per sample)	Equivalent leached thickness (two layers/one layer) for 28.5 wt% NaNO3 (mm)
SO (2.2 MPa, -P)	887	0.43	10.2	1.01/0.51
S4 (4.4 MPa, -P)	872	0.38	9.0	0.90/0.45
S5 (4.4 MPa, +P)	1472	1.06	25.2	2.42/1.21
S7 (3.3 MPa, +P)	805	0.52	12.4	1.23/0.61



Fig. 9. μ CT images: visualization of the hydration front in Eurobitum samples comprised between two stainless steel filters (shown in dark-red) with 28.5 wt% NaNO₃ after (a) 887 days of hydration under a constant stress of 2.2 MPa (22 bar; cell S0) and (b) 1472 days of hydration under a constant stress of 4.4 MPa (44 bar; cell S5). The attenuation values are expressed as 16-bit integers (range 20,000–35,000).

Several observations can be made. Firstly, the central part of the sample consists of a homogeneous mixture of denser and less dense substances. This is the dry Eurobitum. The main part of this layer is made up by (in orange-red represented) material consisting of very small size soluble and sparingly soluble salts (densities of the order of 2-3 g/ml) and (hydr)oxides of Fe, Zr, and Al (densities of 2-5 g/ml) that are intimately mixed with pure bitumen (density 1.03 g/ml). The more 'yellowish' spots are zones with a lower density, probably bitumen with less inorganic material. The few dark-red spots are probably due to locally higher contents of the waste constituents (soluble and sparingly soluble salts, (hydr)oxides of Fe, Zr, and Al, etc.). The central layer of dry Eurobitum is surrounded by two layers with a lower X-ray attenuation value (or: density). These are the (partially) leached layers. Also in these layers, isolated dark-red and orange-red spots can be seen, probably due to the locally higher contents of the waste constituents, where not all NaNO₃ has dissolved yet. In comparison with the dry Eurobitum, more yellow and even green zones are observed

Table 4

Summary of data on the thickness of the leached layer.

(Fig. 9b). The lower attenuation in these places is attributed to (i) the decreasing amount of dry NaNO₃ crystals (density of 2.26 g/ ml) and (ii) the presence of pores filled with NaNO₃ solution (the density of a saturated and a 2 M NaNO3 solution at 25 °C is respectively 1.39 and 1.10 g/ml [19]), of which in addition the diameter is larger then the diameter of the respective pores containing the dry NaNO₃ crystals (for instance, the volume increase upon full dissolution of a NaNO₃ crystal to a saturated NaNO₃ solution is a factor \sim 3.4). From the μ CT images, it is further seen that the thickness of these partially leached layers is not constant over the sample diameter. This is possibly related to the fact that due to the high pressures in these systems some bitumen and/or BW is pressed into the pores of the stainless steel filters, resulting in an extra diffusion limitation for water ingress and salts leaching. Following this idea, the regions with a thinner leached layer would be in contact with a filter zone with more bitumen and/or BW in the pores [30]. The differing thickness of the leached lavers may also be caused by differences in NaNO3 content and crystal size distribution (see Footnote 3). This is very likely also the reason for the observation for sample S5, where the lower leached layer is almost two times thicker than the upper leached layer (Fig. 9b), and for which a higher swelling and cumulative amount of leached NaNO₃ was observed (Figs. 4 and 6).

Furthermore, the overall density of both leached layers is very similar and, at least at first sight, constant over the whole thickness of these layers. The transition between the dry Eurobitum and the leached layers is quite sharp: a few hundred μ m. The total average thickness of the leached layers as determined from the μ CT images is ~2.5 mm (Fig. 9a; cell S0, 887 days at 2.2 MPa) and ~6.2 mm (Fig. 9b; cell S5, 1472 days at 4.4 MPa). The ' μ CT' thicknesses of the leached layers of all analyzed samples are summarized in Table 4. They are systematically higher, by a factor of 2.6–2.9, than the total equivalent leached thickness defined in the previous section. This shows, as expected, that the evolution of the NaNO₃ content (not the dissolved NaNO₃ concentration!) in the leached samples does not change abruptly from zero to its maximum value, *i.e.* no congruent NaNO₃ dissolution and leaching.

Despite the apparently constant density of the leached layer, a closer look at the evolution of the average attenuation in one (vertical) slice, with thickness equal to the voxel size of 94 μ m, reveals that there are attenuation gradients over the leached layer (slices ~200 to ~225) (Fig. 10). The gradient between slices 200 and ~208 is related to the fact that each slice in this layer contains both non-hydrated BW and hydrated BW. The closer to the non-hydrated BW part (*i.e.* closer to slice 200), the more non-hydrated high-density zones are present in the slices, resulting in a higher mean attenuation value. The gradient in mean attenuation value between slices ~208 and ~218 is probably related to a gradient in salt content over the leached layer, and not or much less to a gradient in NaNO₃ concentration in the pore solution, for two reasons:

(1) As already explained, the dissolution of salts results in a larger decrease in density (namely from 2.26 g/ml for dry NaNO₃ to 1.39 g/ml for a saturated NaNO₃ solution at 25 °C) than a dilution of the salt solution (*e.g.* 1.10 g/ml for a 2 M NaNO₃ solution at 25 °C).

Code	Duration (days)	Equivalent leached thickness (two layers / one layer) for 28.5 wt% NaNO ₃ (mm)	Leached thickness based on $\mu CT \ (mm)^a$	Ratio	Leached thickness based on ESEM (mm)	Ratio
S0 (2.2 MPa, -P) S4 (4.4 MPa, -P) S5 (4.4 MPa, +P)	887 872 1472	1.01/0.51 0.90/0.45 2.42/1.21	2.65 2.34 6.29	2.6 2.6 2.6	5.30 5.31 7.09	5.2 5.9 2.9
S7 (3.3 MPa, +P)	805	1.23/0.61	3.53	2.9	3.55	2.9

^a Corrected for the amount of BW in the pores of the two filters.



Fig. 10. Plot of the mean attenuation value per slice parallel to the sample surface in function of the position in the bottom leached layer of sample S5, showing a small attenuation gradient over the leached layer. The thickness of each slice equals 1 voxel size (94 μ m). The attenuation values are expressed as 16-bit integers (range 20,000–35,000).

(2) In addition, as will be discussed in Section 5.2, the (average) NaNO₃ concentration is probably very high over the whole leached layer, except near the outer surfaces.

4.4. ESEM analysis of leached BW

Whereas uCT gives an overall but less detailed view of the leached sample, ESEM of the surface of the cleaved sample (Fig. 11a) yields detailed information on the porosity of a very thin band $(\sim 0.6 \text{ mm width})$, including the transition layer between the dry and the leached part. In Fig. 11b and c two ESEM images of the fracture surface of sample SO are shown. Similar images were obtained for sample S5 and for other samples [30]. Some of the first ESEM analyses were seriously hindered by the adsorption of water vapour by the hygroscopic NaNO3 and the subsequent dissolution (deliquescence, [6,32]), resulting in the appearance – even during the ESEM analysis - of an irregularly shaped 'paste' covering parts of the sample. The use of silicagel during the transport of the samples proved to help to avoid this problem. Typically 30 images were to be taken per sample to map the whole thickness of the ruptured surface, *i.e.* from the upper leached layer (in contact with the filter on the piston) to the lower leached layer (in contact with the filter on the base plate).

The image in Fig. 11b was obtained at the upper outer layer. It has to be noted that for most samples, due to the strong sticking of the swollen sample onto the filters (under a pressure of 2.2-4.4 MPa), (parts of) the outermost leached layers remained stuck on the filters, and could therefore not be scanned. The image in Fig. 11c was taken at the centre of the sample. There is a clear difference between these two images. In the leached layer (Fig. 11b), distinct pores, with a pore diameter varying between \sim 3 and \sim 30 μ m could be seen over nearly the whole scanned surface. The same observations could be made for the many other ESEM images of the leached layers of this and other samples, irrespective of the counterpressure. It was not possible to distinguish any significant difference of the average pore size and the pore size distribution for the four studied samples. At the outermost edge of the sample, which was in contact with the filter, a very thin layer (<100 um) with very low porosity was observed (Fig. 11b). This low permeability layer is believed to be formed by the compression of the outermost leached layer of the sample by the NaNO₃ leaching from this layer in combination with the osmotically-driven transport of water deeper into the sample, and this under the high stress on the sample. In contrast to the leached layer, almost no pores can be seen on the dry part of the sample (Fig. 11c). It is not clear whether the few small pores that can be seen in this image are air-filled pores or NaNO₃ solution containing pores. These latter may locally have formed due to rapid water ingress through small fissures in the sample and/or along the preferential pathways formed by the insoluble but hydrophylic salts and (hydr)oxides [20]. At the scanned surface of the samples, especially at the level of the 'dry' material, but also at the level of the leached layer, crystalline material can be observed, which according to the morphology is NaNO₃. EDX measurements confirm that these crystals mainly consist of NaNO₃, with traces of Ca and S, pointing to the presence of CaSO₄. Thus also in the leached layer undissolved NaNO₃ crystals are still present.

By compiling the 30 ESEM images per sample into one picture – of which the ratio of height and width is too large to include this picture in this paper – it is possible to have a very local view of the whole sample thickness, enabling to determine the local thickness of the leached layer, including the transition layer between dry Eurobitum and the bulk of the leached layer (cfr. Fig. 10). The values of the thickness are also included in Table 4. Considering that for many samples the thickness of the leached layers was not constant over the whole sample – as revealed by the μ CT analysis (Fig. 9) – the 'local' thickness of the leached layers as



Fig. 11. ESEM images of the fracture surface of Eurobitum sample S0, after 887 days of hydration. (a) Visualization of the positions where the ESEM images were recorded. (b) ESEM image of a small area near the sample surface that has been in contact with the leachant solution. (c) ESEM images of a small area in the middle of the sample.

determined from the ESEM analysis corresponds mostly well with the average thickness as determined by μ CT.

5. General discussion and conclusions

In this paper, the swelling of and NaNO₃ leaching from cylindrical non-radioactive Eurobitum bituminized waste samples due to the uptake of water, has been studied in constant stress (or: constant counterpressure; range: 2.2–4.4 MPa) conditions for periods up to about 4 years. During the study, four tests were stopped and the leached samples have been analyzed by micro-focus X-ray Computer Tomography (μ CT) and Environmental Scanning Electron Microscopy (ESEM). The complete set of data enables a consistent interpretation of the observations and leads to an improved understanding of the phenomenology of the water uptake, swelling, and NaNO₃ leaching in restricted swelling conditions.

5.1. Main processes

The results and observations reported in this paper show that the uptake of water by, and the subsequent swelling of bituminized waste with a waste loading of $\sim 40 \text{ wt\%}$ and containing \sim 28 wt% of soluble salts (NaNO₃), are largely controlled by osmosis. Indeed, after about 4 years of contact with water (0.1 mol/L KOH), the swelling varied between \sim 10% and 20%, which is higher than can be explained by recrystallization of the 4-6 wt% of sparingly soluble CaSO₄. In addition, the evolution of the swelling when changing the NaNO₃ concentration in the contacting solution followed the expected behavior of a system controlled by osmosis. The bitumen surrounding the soluble salts and other inorganic compounds proves to behave as a very efficient semi-permeable membrane, especially when submitted to a sufficiently high counterpressure (i.e. swelling in (semi-)confined conditions). The diffusion of NaNO₃ out of the BW combined with the external stress and the osmosis-driven transport of water from the outermost pores with a lower NaNO₃ concentration (higher water activity) towards deeper pores with a higher NaNO₃ concentration (lower water activity), contribute to a local consolidation and the formation of a re-compressed, low porosity layer at both contact sides with the filter. The re-compressed layers in turn contribute to the low permeability of the whole material, and hence to the importance of osmosis as the main process governing the swelling of BW. The fact that after a relatively short initial 'transition' stage the swelling increased almost linearly with time, and not with the square root of time, suggests that in the constant stress conditions in our tests the ingress of water was not the (only) rate-limiting process, and that the observed swelling and swelling rate are the overall result of several transient processes (dissolution, diffusion, advection, creep, involving a low permeability material with evolving thickness and properties) that moreover are non-linear and strongly coupled.

5.2. Average NaNO₃ concentration in the leached layer

Combination of the data on swelling (Section 4.1), cumulative amount of leached NaNO₃ (Section 4.2), thickness of the leached layer as obtained from μ CT and ESEM (Sections 4.3 and 4.4), initial NaNO₃ content in the dry Eurobitum, and density of NaNO₃ and dry Eurobitum, allows to calculate the average NaNO₃ concentration in the leached layer. For the samples S0 and S5 (Fig. 9), the calculated values are 3.8 ± 3.8 M and 3.9 ± 3.9 M, respectively. For the four samples that were already stopped and analyzed, the average NaNO₃ concentration in the leached layer is 4.2 ± 4.2 M (95% confidence interval) (Table 5). It has to be noted that these values are to be reduced by some 10% to 20% to take into account that not all NaNO₃ crystals in the leached layers are dissolved (this fraction can only be roughly estimated, as it is nearly impossible to measure it). The uncertainty on the average NaNO₃ concentration in the leached layer is very high, and is due to the large uncertainties on the sample thickness and the thickness of the leached layers at the end of the water uptake experiment, as obtained from the μ CT images (Fig. 9a and b), and the uncertainty on the total leached amount of NaNO₃ at the end of the water uptake experiment (the effect of the uncertainty on the NaNO₃ content of the sample is not included, but is relatively small).

The fact that according to the ESEM images the leached layers still contain 'solid' NaNO3 might suggest that the NaNO3 concentration in the pores with dissolved NaNO₃ is close to saturation (7.85 M). This is considerably higher, yet not always statistically significantly different, than the calculated average concentrations. It is possible that the bitumen surrounding the undissolved NaNO₃ crystals is locally thicker and/or contains no or less sparingly soluble salts and (hydr)oxides, so that water diffuses extremely slowly towards these crystals. According to this idea, 'islands' with dry, undissolved NaNO3 would exist along with pores containing dissolved NaNO₃, of which the NaNO₃ concentration may vary between saturation and ~ 1 M (for a counterpressure of 4.4 MPa) or \sim 0.5 M (for a counterpressure of 2.2 MPa; see Table A.1). The NaNO₃ that is leached from the BW probably comes from both the nearby and the deeper layers. We have too little insight on the relative contribution of both zones, but the fairly equal distribution of undissolved NaNO3 grains over the whole leached layer suggests that dissolved NaNO₃ also diffuses from the deeper layers to the outer layers. Whatever the exact mechanism, the high and probably nearly constant average NaNO₃ concentration throughout the leached layer is remarkable. It is likely the combined result of (i) the continuous transfer of water deeper into the sample, (ii) the continuous transfer of NaNO₃ from both deeper inside the sample (water hydration front) and from partly dissolved NaNO₃ ('islands') and NaNO₃ solution filled pores in the leached layer, towards the filters, and (iii) the presence of a thin re-compressed layer of leached bitumen that, in addition to the bitumen surrounding the NaNO₃ solution containing pores, behaves as a low permeable and highly efficient semi-permeable membrane.

The values in Table 5 are average concentrations, which are believed to be quite constant over the major part of the leached layer. It is possible that a small concentration gradient exists, with a higher NaNO₃ concentration closer to the dry Eurobitum, and a lower NaNO₃ concentration closer to the outer layer, but this hypothesis cannot be ascertained by analytical results. In any case, the high average dissolved NaNO₃ concentration in most of the leached (or: leaching) layer results in a high (average) osmotic pressure (Appendix A and Table A.1), which is considerably higher than the counterpressures in the test. Only in a very thin layer close to the filter, and insofar as the surrounding bitumen or bituminous material in this layer still behaves as a highly efficient semi-permeable membrane, NaNO₃ solution concentrations might be different for the different counterpressures, with a higher NaNO₃ concentration, and hence a lower dilution (or: swelling), for the higher counterpressure (Table A.1; ~1 mol/L at 4.4 MPa and \sim 0.5 mol/L at 2.2 MPa). This, in combination with at least

Table 5
Average NaNO ₃ concentration in the leached layers of the four dismantled samples

Code	Duration (days)	Average NaNO3 concentration (mol/L)		
SO (2.2 MPa, -P)	887	3.8 ± 3.8		
S4 (4.4 MPa, -P)	872	3.9 ± 3.9		
S5 (4.4 MPa, +P)	1472	4.4 ± 4.4		
S7 (3.3 MPa, +P)	805	4.4 ± 4.4		
Average		4.2 ± 4.2		

two sources of variability (local variability of the NaNO₃ content and related pore size distribution; bitumen or bituminous material behaving locally more or less as a highly efficient semi-permeable membrane) and the small difference in pore size for a twofold dilution, explains why there is no measurable effect of the counterpressure on the swelling, at least not in the range of counterpressures applied in this study.

5.3. Phenomenology of the swelling in restricted swelling conditions and expected evolution of the system

From the above, it is concluded that the phenomenology of the water uptake, swelling, and salts leaching in restricted swelling conditions differs considerably from what is observed for the free swelling (Fig. 2), where a steady increase of the pore size is observed, for which a steady decrease of the NaNO₃ concentration is postulated [8,11,12]. Fig. 12 presents schematically the phenomenology of the water uptake and swelling in restricted swelling (constant stress) conditions for a binary mixture of bitumen and NaNO₃.

We intend to continue to monitor some of the remaining water uptake tests until the swelling stops. Based on the data reported in this work, it can be expected that it will take still several years before the hydration front has reached the centre of the samples in the remaining water uptake tests, and it will require even more time before all NaNO₃ has dissolved. During some part of this time the samples will continue to swell. We can only speculate about when and how the swelling will finally stop. We expect that at some point in time a further volume increase due to the water uptake by the dry NaNO3 crystals and/or the dilution of the concentrated NaNO₃ solutions in the pores will be increasingly more compensated by a re-compression of the leached layer, causing the swelling to level off before dissolution of all NaNO3 and/or advanced dilution of the concentrated NaNO₃ solution. Finally, when all NaNO₃ will be dissolved and the average NaNO₃ concentration in the BW will start to decrease, the related osmotic pressure will decrease accordingly, and eventually nearly full recompression of the leached BW is expected to occur. Depending on the osmotic efficiency of the re-compressed material, this may take a very long time. A similar phenomenology is anticipated for a full-scale drum with Eurobitum, yet with different kinetics, a.o. because of the effect of ageing of the bitumen [23-25]. From a safety point of view, it is important to know at which swelling degrees the BW will stop to swell, as this determines the maximum volumetric deformation of the host formation (this latter depends also on the stress–strain relationship (constitutive model) of the host clay, which is also a subject of ongoing research). It can be noted here that for bituminized waste with a waste loading of ~50 wt% or higher (*i.e.* the percolation threshold [21,22]) the formation of a thick re-compressed leached layer might result in the osmosis-induced swelling of the remainder of such bituminized waste product.

The observations reported in this paper (swelling, NaNO₃ leaching, linear increase of the swelling and NaNO₃ leaching with time, absence of an important effect of the counterpressure on the swelling in the studied range (2.2-4.4 MPa), formation and growth of a low porosity - low permeability outer layer) can be reproduced well with the fully coupled chemo-hydro-mechanical constitutive model for Europitum, developed by the International Centre for Numerical Methods and Engineering (CIMNE - Polytechnical University of Cataluña, Barcelona, Spain), and many results are presented in [18]. For this model the balance equations for water, dissolved salts, crystals and solid phase were written with taking into account the coupled flows, namely osmotic flow and ultrafiltration, and the dissolution/precipitation of salts. The balance equations are coupled to the equilibrium of stresses, and the formulation has been included as an extension in a coupled thermohydro-mechanical program (code Bright[®]).

An important objective of the ongoing research program is to be able to make sound predictions regarding the interaction between the swelling Eurobitum and the surrounding Boom Clay, to support the decision about the number of waste drums that can be placed per meter of gallery without risking an unacceptably high deformation and hence perturbation of the host formation. The improved understanding of the phenomenology of the water uptake, swelling, and NaNO₃ leaching in restricted swelling conditions, integrated in the fully coupled CHM constitutive model, offers good perspectives to achieve this goal.

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Fig. 12. Simplified schematic representation of the water uptake and swelling in a binary bitumen – NaNO₃ mixture in constant stress (restricted) swelling conditions. (a) Dry mixture of bitumen and NaNO₃ crystals. (b) Mixture in which in the first layers most of the NaNO₃ crystals are partially or completely dissolved (to an oversaturated, saturated, or undersaturated solution). (c) Mixture such as in (b), but with a re-compressed low permeable layer. \Box = dry NaNO₃ crystal, \bigcirc = pore with NaNO₃ solution, filter (and, not drawn, piston) at a given counterpressure. \downarrow refers to the direction of water taken up by the material, \bigcirc refers to the direction of the swelling.

Materials, as part of its programme on geological disposal of medium-level long-lived waste.

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Appendix A

The osmotic pressure Π can be considered as the pressure that needs to be exerted on a solution to prevent osmosis-driven flow of solvent into that solution when it is separated from the pure solvent by a semi-permeable membrane. Conversely, it can be considered as the pressure that is exerted by such solution when osmosis-driven flow of solvent, and related volume increase, is made impossible (*i.e.* constant volume). The osmotic pressure can be calculated on the basis of the following equation [31]:

$$\Pi = \frac{R \cdot T}{\nu_{\rm H_2O}} \cdot \ln \left(\frac{p_{\rm H_2O}^0}{p_{\rm H_2O}} \right)$$
(2)

in which *R* is the ideal gas constant (0.0821 L atm/K mol or 8.314 J/ K mol), *T* the temperature (K; 25 °C = 298.15 K), $v_{H_{2}0}$ the partial molar volume of water (L/mol), $p_{H_{2}0}^0$ the water vapour pressure of pure water and $p_{H_{2}0}$ the water vapour pressure above the salt solution (*e.g.* mm). The ratio of $p_{H_{2}0}$ and $p_{H_{2}0}^0$ is the water activity. For a saturated NaNO₃ solution at 25 °C (7.8457 mol/L), the water activity equals 0.74 [19], and the corresponding osmotic pressure is as high as 422 atm (428 bar or 43 MPa). The osmotic pressure decreases with increasing water activity (or: decreasing NaNO₃ concentration). For a given amount of NaNO₃ surrounded by a semipermeable membrane that can stretch whilst maintaining its membrane properties, a lower NaNO₃ concentration means a higher degree of dilution, hence a higher degree of swelling. Table A.1 gives

Table A.1

NaNO₃

Water vapour pressure (mm Hg), water activity, and osmotic pressure (MPa) calculated for different NaNO₃ solution concentrations (mol/L) at 25 $^\circ$ C [19,31].

Water activity Osmotic pressure (MPa)

Water vapour

concentration (mol/L)	pressure (mm Hg)			
Osmotic pressur [19]	res calculated with Ec	ı. (2) using the a	lata of Pearce and Hopson	
7.85	17.554	0.739	42.8	
7.41	17.957	0.756	39.6	
6.86	18.448	0.777	35.7	
6.27	18.987	0.799	31.6	
5.65	19.484	0.820	27.9	
4.99	19.999	0.842	24.2	
4.28	20.534	0.865	20.5	
3.53	21.092	0.888	16.7	
2.73	21.691	0.913	12.7	
2.31	21.998	0.926	10.7	
1.88	22.332	0.940	8.6	
1.43	22.650	0.954	6.6	
0.97	23.006	0.969	4.4	
0.78	23.152	0.975	3.5	
0.59	23.299	0.981	2.7	
0.39	23.446	0.987	1.8	
0.20	23.596	0.993	0.9	
0.10	23.674	0.997	0.5	
0.00	23.752	1.000	0.0	
Osmotic pressures calculated with $Y = 0.654 \cdot x^2 + 44.758 \cdot x$ ($R^2 = 1$), with $x = NaNO_3$ solution concentration (mol/L), obtained by fitting part of the above				
0 97	Not calculated	Not calculated	4 4	
/		concondicu		

the osmotic pressures calculated according to Eq. (2) for the water vapour pressures measured by Pearce and Hopson [19], as well as some specific values that were calculated after fitting the osmotic pressure – $NaNO_3$ solution concentration relationship of the primary data in the table.

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data (range 0–3.53 mol/L) with a second order polynomial						
0.97	Not calculated	Not calculated	4.4			
0.73	Not calculated	Not calculated	3.3			
0.49	Not calculated	Not calculated	2.2			